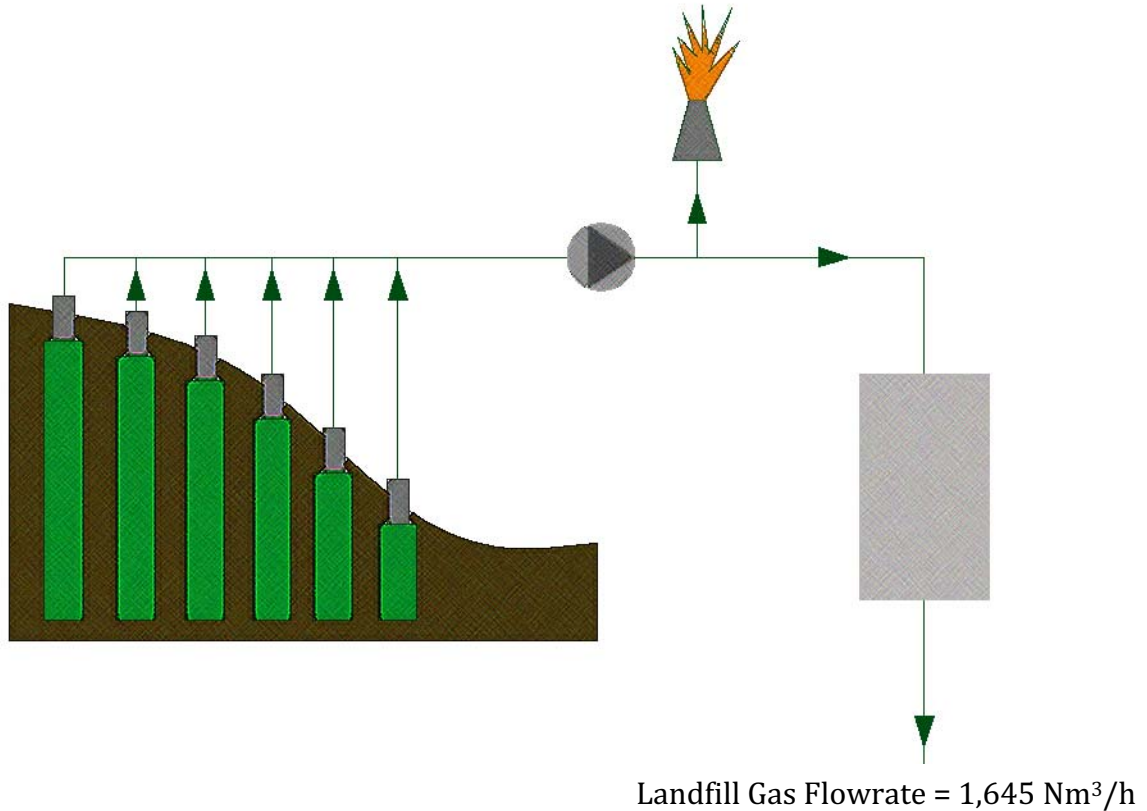


Appendix D: Sample Redesign Calculations

GROWS Inc. Landfill



Approximate Size: 4,053,804 ft²

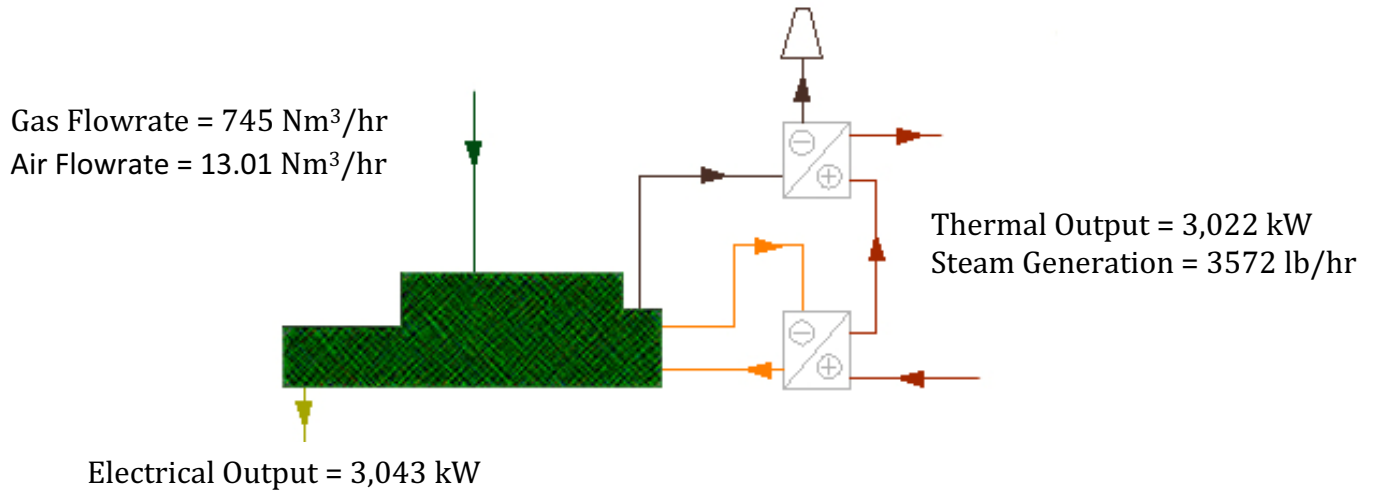
Average Gas Production* = 0.344 scf/ ft²/day

Landfill Gas = (4,053,804 ft²) x (0.344 scf/ ft²/day) / (24 hours) = 58,104 scf/hr

Landfill Gas Produced = (58,104 scf/hr) = **1,645 Nm³/h**

*Sources: Waste Management http://www.americanlandfill.com/facility/gas_to_energy.asp
<http://www.mrwmd.org/landfill-gas-power.htm>

Engine: Jenbacher JMS 620 GS- NL



Natural Gas:

Natural Gas Volume Flowrate = 745 Nm³/hr

Fuel Lower Heating Value = 9.5 kWh/Nm³

Electrical Efficiency = 43.0%

Thermal Efficiency = 42.7%

Total Efficiency = 85.7%

Exhaust Gas to HX = 41.6%

Exhaust Gas Volume Flowrate = 13.66 Nm³/hr

Full Load Exhaust Gas Temperature = 425°C

Steam Generated Pressure = 125 psig

Steam Total Heat = 1,193 (Btu/lb)

Combustion Air Volume Flowrate = 13.01 Nm³/hr

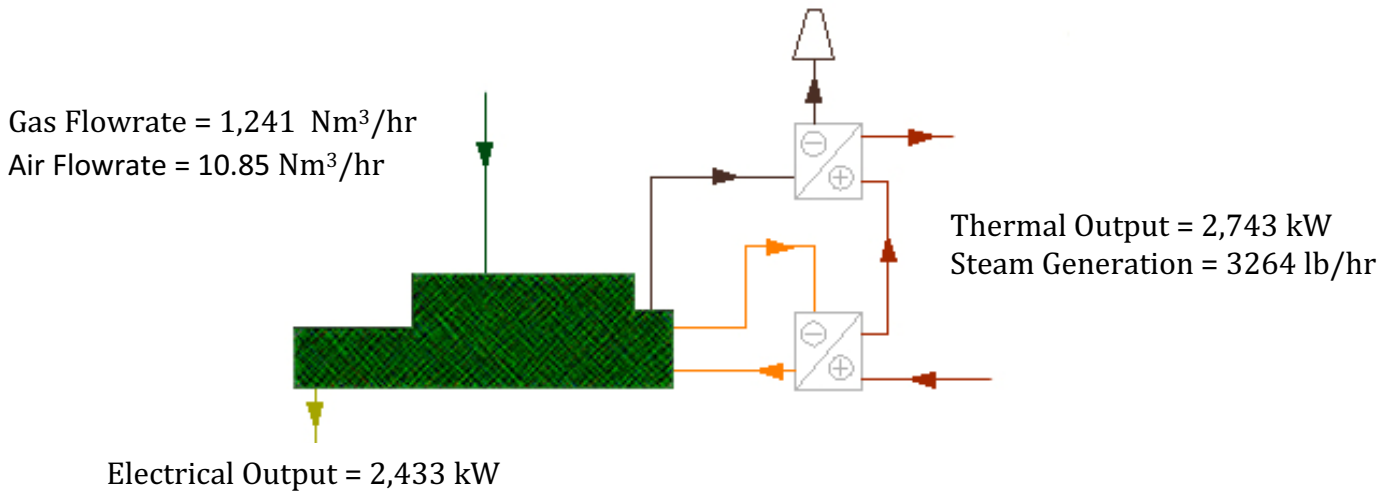
Hot Water Volume Flowrate = 129.7 m³/hr

Max Electrical Output = (745 Nm³/hr) x (9.5 kWh/Nm³) x (0.43) = **3,043 kW**

Max Thermal Output = (745 Nm³/hr) x (9.5 kWh/Nm³) x (0.427) = **3,022 kW**

Steam Generation = (3,002 kW) x (3,412 Btu/hr/kW) / (1193 Btu/lb) x (0.416)
= **3572 lb/hr**

Engine: Jenbacher JMS 620 GS- BL



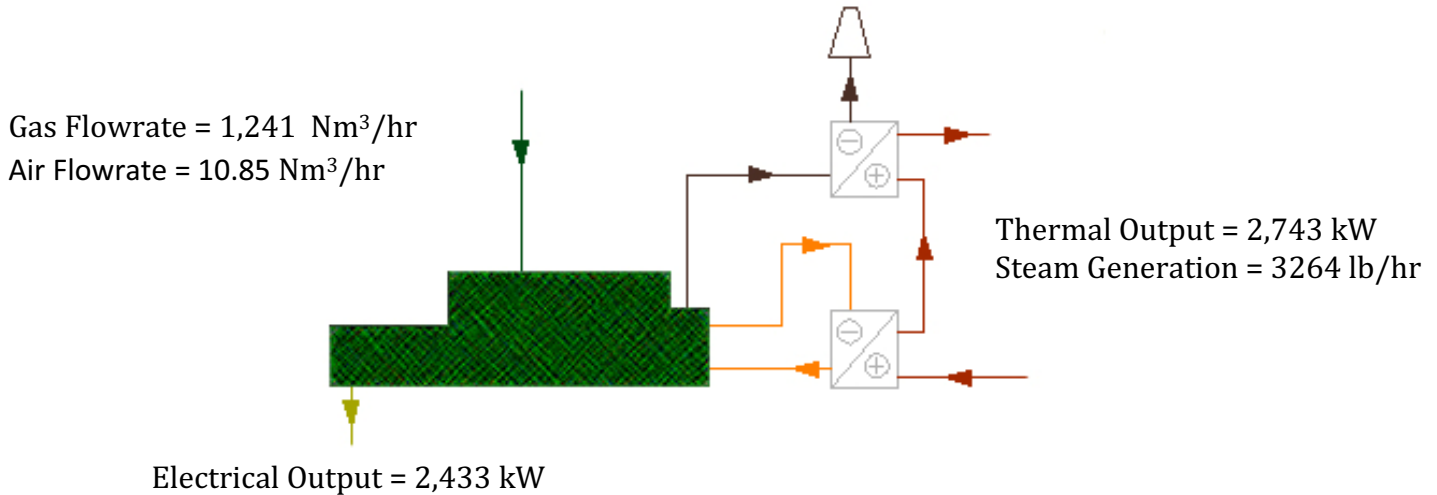
Landfill Gas:

Landfill Gas Volume Flowrate = 1,241 Nm³/hr
 Fuel Lower Heating Value = 5 kWh/Nm³
 Electrical Efficiency = 39.2%
 Thermal Efficiency = 44.2%
 Total Efficiency = 83.4%
 Exhaust Gas to HX = 41.6%
 Exhaust Gas Volume Flowrate = 11.78 Nm³/hr
 Maximum Demand Exhaust Gas Temperature = 467°C
 Steam Generated Pressure = 125 psig
 Steam Total Heat = 1,193 Btu/lb
 Combustion Air Volume Flowrate = 10.85 Nm³/hr
 Hot Water Volume Flowrate = 78.5 m³/hr

Summer

Max Electrical Output = (1,241 Nm³/h) x (5 kWh/Nm³) x (0.392) = **2,433 kW**
 Max Thermal Output = (1,241 Nm³/h) x (5 kWh/Nm³) x (0.442) = **2,743 kW**
 Amount of Flared Gas = (1,645 Nm³/h) - (1,241 Nm³/h) = **404 Nm³/hr**
 Max Steam Generation = (2,743 kW) x (3,412 Btu/h/kW) / (1193 Btu/lb) x (0.416)
 = **3264 lb/hr**
 Min Fuel Input = (2,407 kW) / (5 kWh/Nm³) / (0.392) = **1,228 Nm³/hr**
 Min Thermal Output = (1,228 Nm³/h) x (5 kWh/Nm³) x (0.442) = **2,714 kW**
 Min Steam Generation = (2,714 kW) x (3,412 Btu/h/kW) / (1193 Btu/lb) x (0.416)
 = **3,229 lb/hr**

Engine: Jenbacher JMS 620 GS- BL (cont.)



Winter

$$\text{Max Fuel Input} = (1,855 \text{ kW}) / (5 \text{ kWh/Nm}^3) / (0.392) = \mathbf{946 \text{ Nm}^3/\text{hr}}$$

$$\text{Max Thermal Output} = (946 \text{ Nm}^3/\text{h}) \times (5 \text{ kWh/Nm}^3) \times (0.442) = \mathbf{2,092 \text{ kW}}$$

$$\begin{aligned} \text{Max Steam Generation} &= (2,092 \text{ kW}) \times (3,412 \text{ Btu/h/kW}) / (1193 \text{ Btu/lb}) \times (0.416) \\ &= \mathbf{2489 \text{ lb/hr}} \end{aligned}$$

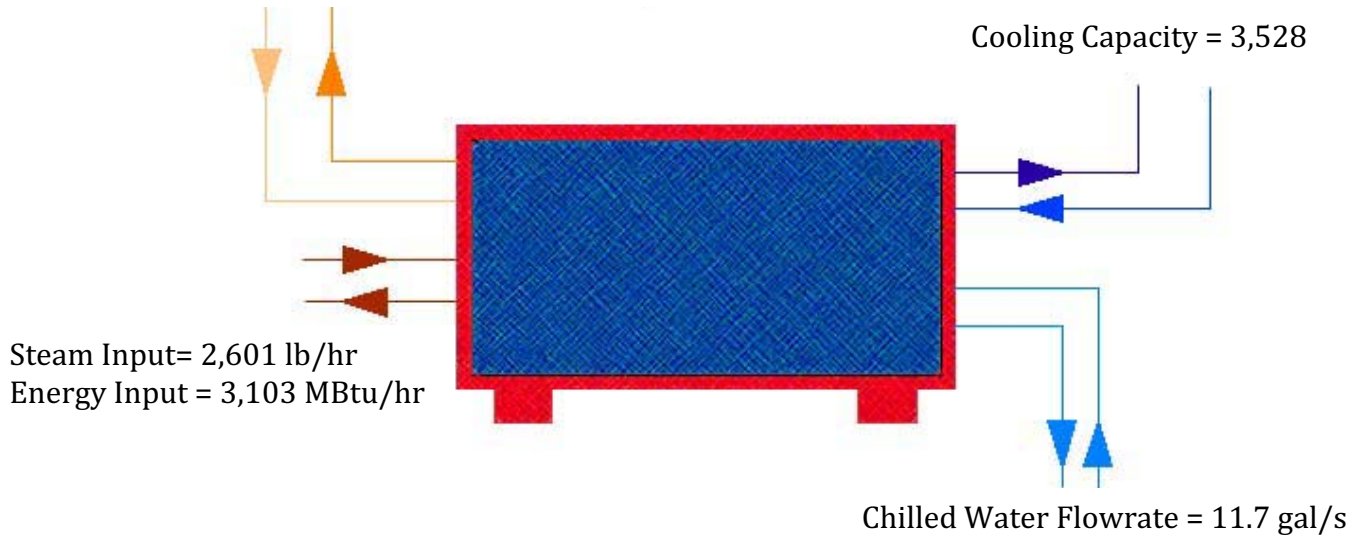
$$\text{Min Fuel Input} = (1,832 \text{ kW}) / (5 \text{ kWh/Nm}^3) / (0.392) = \mathbf{935 \text{ Nm}^3/\text{hr}}$$

$$\text{Min Thermal Output} = (935 \text{ Nm}^3/\text{h}) \times (5 \text{ kWh/Nm}^3) \times (0.442) = \mathbf{2,066 \text{ kW}}$$

$$\begin{aligned} \text{Min Steam Generation} &= (2,066 \text{ kW}) \times (3,412 \text{ Btu/h/kW}) / (1193 \text{ Btu/lb}) \times (0.416) \\ &= \mathbf{2458 \text{ lb/hr}} \end{aligned}$$

Absorption Chiller/Heater: Carrier 16NK

Heating Capacity = 3,103 MBtu/hr



Double-Effect and Steam Fired

Cooling Capacity = 1034 kW = 294 Tons = 3,528,000 Btu/hr

Chilled Water Volume Flowrate = 44.4 L/s = 11.7 gal/s

Cooled Water Temperature = 45°F

Cooled Water Volume Flowrate = 74.2 L/s = 1,176 gpm

Steam Consumption = 1180 kg/h = 2601 lb/hr

Energy Input = (2,601 lb/hr) x (1,193 Btu/lb) = **3,103 MBtu/hr**

Energy Output = **3,528 MBtu/hr**

COP = (3,528 MBtu/hr) / (3,103 MBtu/hr) = **1.14**

Cooling

Full Load Demand

Engine Steam Produced = **3,264 lb/hr**

Chiller Steam Consumption = **2,601 lb/hr**

Excess Steam = (3264 lb/hr) - (2601 lb/hr) = **663 lb/hr**

Partial Load Demand

Engine Steam Produced = **3,229 lb/hr**

Chiller Steam Consumption = **2601 lb/hr**

Peak Steam Consumption = **2,601 lb/hr**

Excess Steam = (3264 lb/hr) - (2601 lb/hr) = **628 lb/hr**

(Even at the minimum demand there is still enough steam to meet the maximum cooling load, therefore a standby centrifugal chiller is not needed.)

Heating

Minimum Load Demand

Engine Steam Produced = **2458 lb/hr**

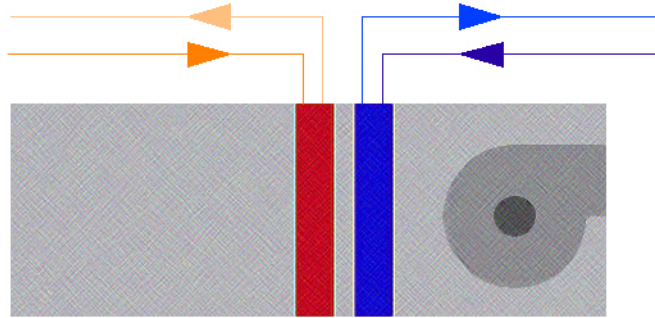
Steam Capacity = (2458 lb/hr) x (1,193 Btu/lb) = **2,932 MBtu/hr**

Peak Heating Demand = **1,239 MBtu/hr**

Excess Steam Capacity = (2,932 MBtu/hr) - (1,239 MBtu/hr) = **1693 MBtu/hr**

(Even at the minimum electrical demand there is still enough steam to meet the maximum heating load, therefore a standby gas-fired boiler is not needed.)

Rooftop Unit A1: TRANE Rooftop Unit



Peak Cooling = 77 tons
 Peak Heating = 337 MBtu/hr
 Peak Supply = 29,477 cfm
 Peak Return = 24,761 cfm
 Peak Outside Air = 16%
 Total Static Pressure = 2.0 inches
 Return Static Pressure = 0.8 inches

Step 1: Casing Size

Peak Heating = 337 MBtu/hr from Table GD-1 **Casing 2** is selected

Step 2: Supply and Exhaust Fan

Peak Supply = 29,477 cfm and External Static Pressure = 2.0 inches
 a **supply fan at 25 bhp and 1043 rpm** is selected

Peak Return = 24,761 cfm and Return Static Pressure = 0.8 inches
 an **exhaust fan at 10 bhp and 750 rpm** is selected

Step 3: Hot Water Heating System

Supply Fan Heat = (25 bhp x 2.8) = **70 Mbtu/hr**

Supply Fan Temperature Rise = 70,000 Btu / (1.085 x 29,477 cfm) = **2.19°F**

Mixed Air Temperature = 70°F + (0.16)(0°F - 70°F) = **58.8°F**

Total Winter Heating Load = 337 MBtu/hr - 20.3 Mbtu/hr = **316.7 Mbtu/hr**

Steam Needed = (316,700 Btu/hr) / (1,193 Btu/lb) = **265.5 lb/hr**

Steam Remaining = (2458 lb/hr) - (265.5 lb/hr) = **2192.5 lb/hr**

Step 4: Chilled Water Cooling System

Peak Cooling = 77 tons = **924,000 Btu/hr**

Water Leaving Temperature = $[(924,000 \text{ Btu/hr}) / (500) / (2.94 \text{ gpm})] + 45^\circ\text{F} = \mathbf{51^\circ\text{F}}$

$\Delta T_L = 90^\circ\text{F} - 51^\circ\text{F} = 39^\circ\text{F}$

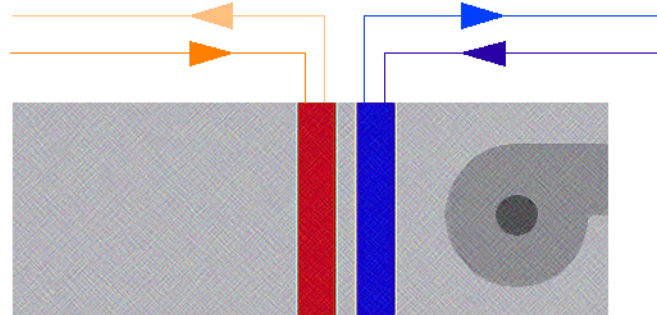
$\Delta T_S = 55^\circ\text{F} - 45^\circ\text{F} = 10^\circ\text{F}$

LMTD = **21.3°F** (From LMTD Table)

Capacity = 232,000 Btu/hr/row (Coil selection chart)

Rows = $(924,000 \text{ Btu/hr}) / (232,000 \text{ Btu/hr/row}) = 3.98 \text{ rows} = \mathbf{4 \text{ Rows}}$

Rooftop Unit A2: TRANE Rooftop Unit



Peak Cooling = 108 tons
 Peak Heating = 647 MBtu/hr
 Peak Supply = 36,318 cfm
 Peak Return = 27,239 cfm
 Peak Outside Air = 25%
 Total Static Pressure = 2.0 inches
 Return Static Pressure = 0.8 inches

Step 1: Casing Size

Peak Heating = 647 MBtu/hr from Table GD-1 **Casing 4** is selected

Step 2: Supply and Exhaust Fan

Peak Supply = 36,318 cfm and External Static Pressure = 2.0 inches
 a **supply fan at 30 bhp and 1150 rpm** is selected

Peak Return = 27,239 cfm and Return Static Pressure = 0.8 inches
 an **exhaust fan at 15 bhp and 1000 rpm** is selected

Step 3: Hot Water Heating System

Supply Fan Heat = (30 bhp x 2.8) = **84 Mbtu/hr**

Supply Fan Temperature Rise = 84,000 Btu / (1.085 x 29,477 cfm) = **2.63°F**

Mixed Air Temperature = 70°F + (0.25)(0°F - 70°F) = **52.5°F**

Total Winter Heating Load = 647 MBtu/hr - 84 Mbtu/hr = **563 Mbtu/hr**

Steam Needed = (563,000 Btu/hr) / (1,193 Btu/lb) = **472 lb/hr**

Steam Remaining = (2192.5 lb/hr) - (472 lb/hr) = **1721 lb/hr**

Step 4: Chilled Water Cooling System

Peak Cooling = 108 tons = **1,296,000 Btu/hr**

Water Leaving Temperature = $[(1,296,000 \text{ Btu/hr}) / (500) / (2.94 \text{ gpm})] + 45^\circ\text{F} = \mathbf{54^\circ\text{F}}$

$\Delta T_L = 90^\circ\text{F} - 54^\circ\text{F} = 36^\circ\text{F}$

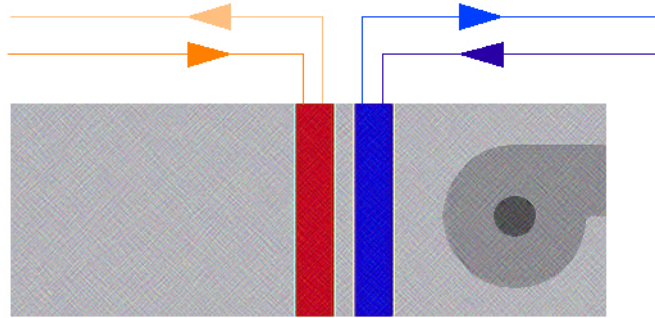
$\Delta T_S = 55^\circ\text{F} - 45^\circ\text{F} = 10^\circ\text{F}$

LMTD = **19.5°F** (From LMTD Table)

Capacity = 232,000 Btu/hr/row (Coil selection chart)

Rows = $(1,296,000 \text{ Btu/hr}) / (232,000 \text{ Btu/hr/row}) = 5.58 \text{ rows} = \mathbf{6 \text{ Rows}}$

Rooftop Unit A3: TRANE Rooftop Unit



Peak Cooling = 42 tons
 Peak Heating = 140 MBtu/h
 Peak Supply = 17,615 cfm
 Peak Return = 15,854 cfm
 Peak Outside Air = 10%
 Total Static Pressure = 1.5 inches
 Return Static Pressure = 0.6 inches

Step 1: Casing Size

Peak Heating = 140 MBtu/hr from Table GD-1 **Casing 2** is selected

Step 2: Supply and Exhaust Fan

Peak Supply = 17,615 cfm and External Static Pressure = 1.5 inches
 a **supply fan at 11 bhp and 800 rpm** is selected

Peak Return = 15,854 cfm and Return Static Pressure = 0.6 inches
 an **exhaust fan at 6 bhp and 700 rpm** is selected

Step 3: Hot Water Heating System

Supply Fan Heat = (11 bhp x 2.8) = **31 Mbtu/hr**

Supply Fan Temperature Rise = 31,000 Btu / (1.085 x 17,615 cfm) = **1.62°F**

Mixed Air Temperature = 70°F + (0.10)(0°F - 70°F) = **63°F**

Total Winter Heating Load = 140 MBtu/hr - 31 Mbtu/hr = **109 Mbtu/hr**

Steam Needed = (109,000 Btu/hr) / (1,193 Btu/lb) = **91 lb/hr**

Steam Remaining = (1721 lb/hr) - (91 lb/hr) = **1630 lb/hr**

Step 4: Chilled Water Cooling System

Peak Cooling = 42 tons = **504,000 Btu/hr**

Water Leaving Temperature = $[(504,000 \text{ Btu/hr}) / (500) / (2.94 \text{ gpm})] + 45^\circ\text{F} = \mathbf{48^\circ\text{F}}$

$\Delta T_L = 90^\circ\text{F} - 48^\circ\text{F} = 42^\circ\text{F}$

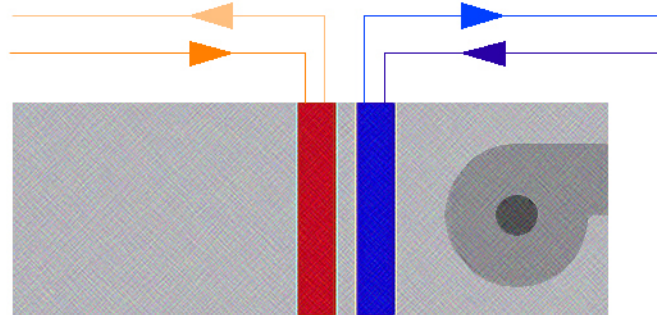
$\Delta T_S = 55^\circ\text{F} - 45^\circ\text{F} = 10^\circ\text{F}$

LMTD = **22.25°F** (From LMTD Table)

Capacity = 232,000 Btu/hr/row (Coil selection chart)

Rows = $(504,000 \text{ Btu/hr}) / (232,000 \text{ Btu/hr/row}) = \mathbf{2 \text{ Rows}}$

Rooftop Unit A4: TRANE Rooftop Unit



Peak Cooling = 40 tons
 Peak Heating = 117 MBtu/h
 Peak Supply = 16,553 cfm
 Peak Return = 14,898 cfm
 Peak Outside Air = 10%
 Total Static Pressure = 1.5 inches
 Return Static Pressure = 0.6 inches

Step 1: Casing Size

Peak Heating = 117 MBtu/hr from Table GD-1 **Casing 2** is selected

Step 2: Supply and Exhaust Fan

Peak Supply = 16,553 cfm and External Static Pressure = 1.5 inches
 a **supply fan at 11 bhp and 800 rpm** is selected

Peak Return = 14,898 cfm and Return Static Pressure = 0.6 inches
 an **exhaust fan at 6 bhp and 700 rpm** is selected

Step 3: Hot Water Heating System

Supply Fan Heat = (11 bhp x 2.8) = **31 Mbtu/hr**

Supply Fan Temperature Rise = 31,000 Btu / (1.085 x 16,553 cfm) = **1.73°F**

Mixed Air Temperature = 70°F + (0.10)(0°F - 70°F) = **63°F**

Total Winter Heating Load = 117 MBtu/hr - 31 Mbtu/hr = **86 Mbtu/hr**

Steam Needed = (86,000 Btu/hr) / (1,193 Btu/lb) = **72 lb/hr**

Steam Remaining = (1,630 lb/hr) - (72 lb/hr) = **1,558 lb/hr**

Step 4: Chilled Water Cooling System

Peak Cooling = 40 tons = **480,000 Btu/hr**

Water Leaving Temperature = $[(480,000 \text{ Btu/hr}) / (500) / (2.94 \text{ gpm})] + 45^\circ\text{F} = \mathbf{48^\circ\text{F}}$

$\Delta T_L = 90^\circ\text{F} - 48^\circ\text{F} = 42^\circ\text{F}$

$\Delta T_S = 55^\circ\text{F} - 45^\circ\text{F} = 10^\circ\text{F}$

LMTD = **22.25°F** (From LMTD Table)

Capacity = 232,000 Btu/hr/row (Coil selection chart)

Rows = $(480,000 \text{ Btu/hr}) / (232,000 \text{ Btu/hr/row}) = \mathbf{2 \text{ Rows}}$